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What is claimed is:

- 1. A catalyst for removing dioxin, comprising 1-10 wt% of vanadium, 0.1-5 wt% of nickel, 0.1-5 wt% of molybdenum and 1-15 wt% of tungsten, on a mixture support consisting essentially of 10-50 wt% of alumina and 50-90 wt% of titania.
 - 2. A method for preparing a dioxin removal catalyst, which comprises the following steps of:
- a) pretreating a spent catalyst discharged from a hydro-desulfurization process of an oil refinery, which comprises 5-30 wt% of vanadium; 1-10 wt% of nickel, 1-10 wt% of molybdenum, 0.1-5 wt% of iron, 1-10 wt% of sulfur, 0.1-5 wt% of silicon and 0.1-5 wt% of phosphor on an alumina support by thermally treating said spent catalyst, followed by washing with water;
 - b) providing a titania impregnated with 1 to 20 wt% of tungsten;
- c) homogeneously mixing the pretreated spent catalyst 20 with the tungsten-impregnated titania under the addition of water and acid;
 - d) dehydrating the mixture to remove excess moisture and active metal components therein;
- e) drying the dehydrated mixture, followed by grinding 25 the dried mixture; and

- f) forming a catalyst body by extruding the grinded mixture or coating the grinded mixture to a structure, followed by drying and then calcining the dried structure.
- 3. The method as defined in claim 2, wherein the thermally treating of the a) step is carried out at 300-400 °C for 3-5 hours.
- 4. The method as defined in claim 2, wherein the tungsten-impregnated titania has a specific surface area of $60\text{--}100~\text{m}^2/\text{g}$ and pore sizes of 150--200~Å, and has anatase crystalline structure.
- 5. The method as defined in claim 2, wherein the alumina support in the spent catalyst is a gamma alumina support, and has a specific surface area of $40-100 \text{ m}^2/\text{g}$ and pore sizes of 150-300 Å.
- 6. The method as defined in claim 2, wherein the acid is oxalic acid or citric acid and is added at an amount of 3 to 7 wt% based on the spent catalyst and the tungsten-impregnated titania in the c) step.
- 7. The method as defined in claim 2, the c) step is carried out in the ball mill until 2-3 μm particles amount

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to 40-60 vol%.

- 8. The method as defined in claim 2, wherein the spent catalyst and the tungsten-impregnated titania are mixed at weight ratio of 10:90-50:50 in the c) step.
 - 9. The method as defined in claim 2, wherein the d) step is carried out by use of a filter press under a pressure of $10-15 \text{ kg/cm}^2$.

10. The method as defined in claim 2, wherein the e)

step is conducted by use of a continuous dryer-miller.

- 11. The method as defined in claim 2, wherein the drying of the e) step is carried at 80-120 $^{\circ}$ C for 0.5-2 hours.
- 12. The method as defined in claim 2, wherein the drying of the f) step is carried by use of hot blast dryer,
 20 microwave dryer or thermohydrostat at 60-120 °C for 3-48 hours.
- 13. The method as defined in claim 2, wherein the calcining of the f) step is carried at 450-550°C for 3-5 hours.

14. The method as defined in claim 2, wherein the extruding comprises dry-mixing the grinded mixture with organic binders, inorganic binders and glass fiber; aging the dry-mixture, together with water, plasticizers, lubricants and dispersants, at 5 °C or lower for 1-2 days; kneading the aged mixture in a kneader 2-5 times; storing said kneaded mixture at 5 °C or lower for 1-5 days; and molding the stored mixture into a honeycomb form through a vacuum extruder.

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15. The method as defined in claim 2, wherein the coating comprises applying, pouring or pressure-adhering a coating material including the grinded mixture, inorganic binders and water to a metal plate of honeycomb form or a cordierite-typed ceramic honeycomb.